

# Safety analysis on beam dump

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*Safety group*

SSTAC meeting, July 23, 2015

# Topics:

1. *Overview on Beam Dump*
2. *Description of cooling circuit*
3. *Safety philosophy*
4. *BD safety system: definition of shut-down signals*
5. *Critical safety aspects: accident scenario*

# Overview on Beam Dump

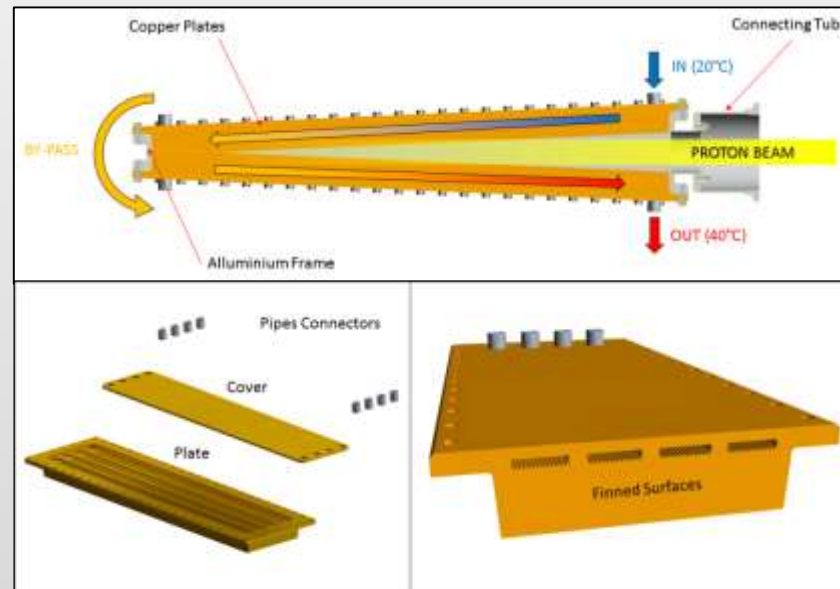
Ref. E. Boratto

## INPUT

Water properties  
at reference T:  
 $\rho, \mu, c, \lambda$

Hydraulic properties:  
 $Q_{\text{tot}} = 2400 \text{ l/h}$   
 $v = 1,25 \text{ m/s}$

**Heat Dissipation  $P = 52,5 \text{ kW}$**

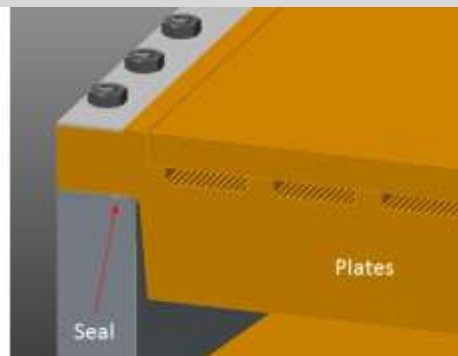
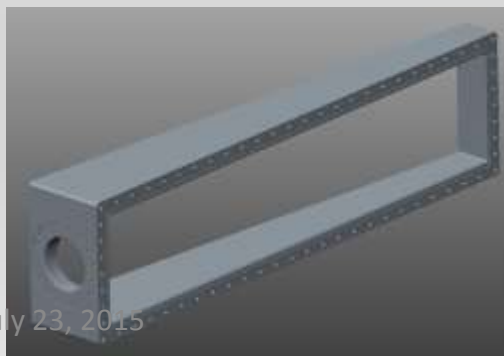


## OUTPUT

Fluid dynamic  
parameters:  
 $Re, Nu, Pr$



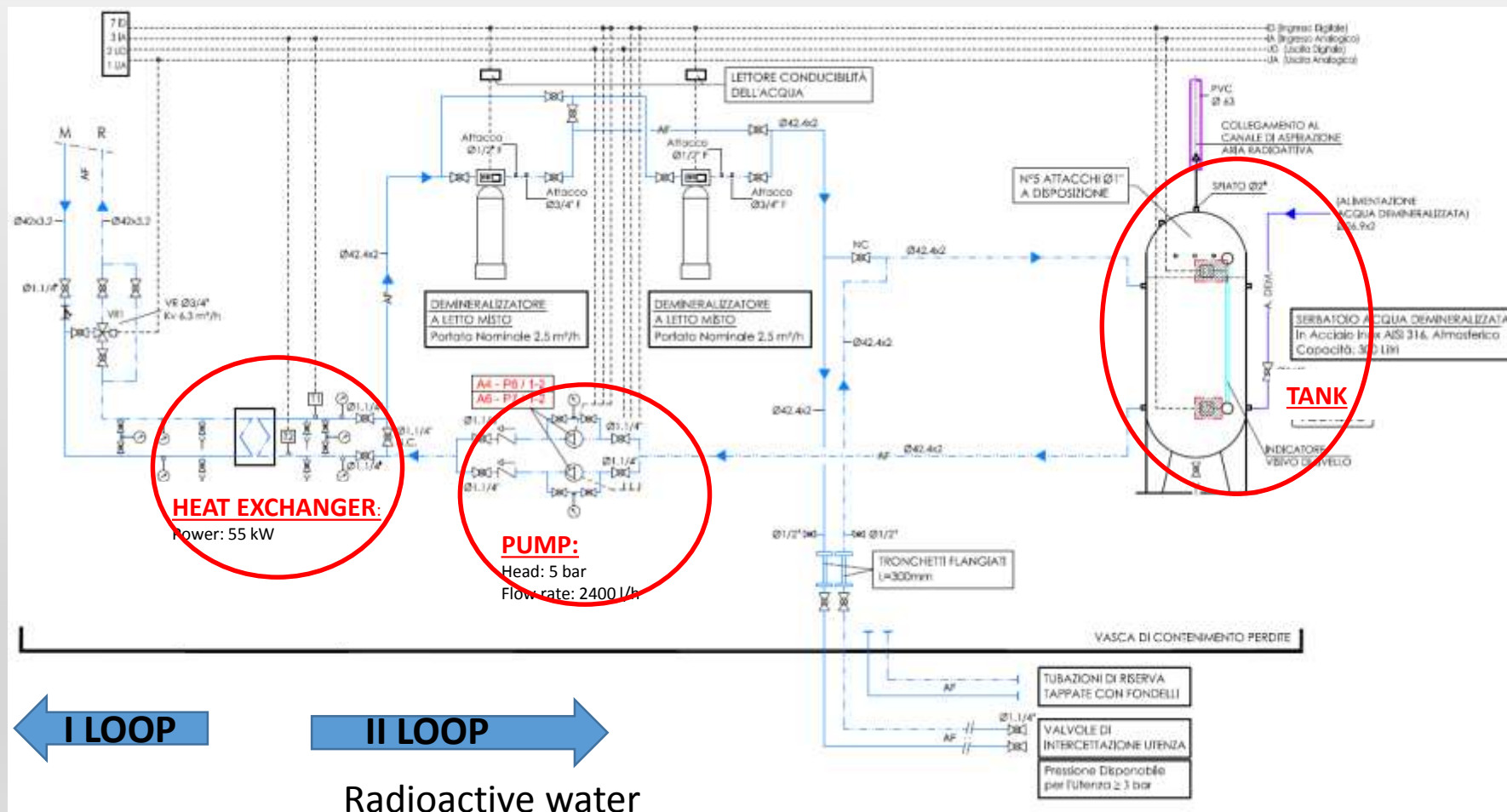
$\Delta t = 20^\circ \text{ C}$   
 $HTC = 7000 \text{ W m}^{-2}\text{K}$   
(dittus-boelter)



*The vacuum is ensured by suitable **INDIUM** gaskets disposed along the perimeter of the Al grafts.*

# Description of cooling circuit

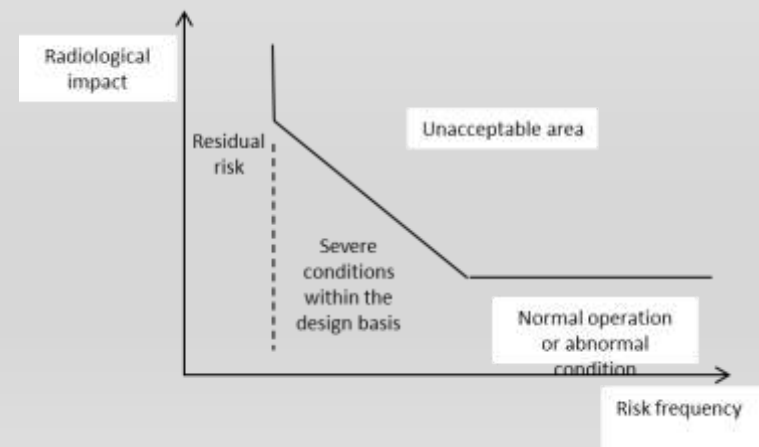
## Provisional lay out



# Safety philosophy (1)

**Safety functions** (International Nuclear Safety Advisor Group 12 - IAEA) **adapted to SPES:**

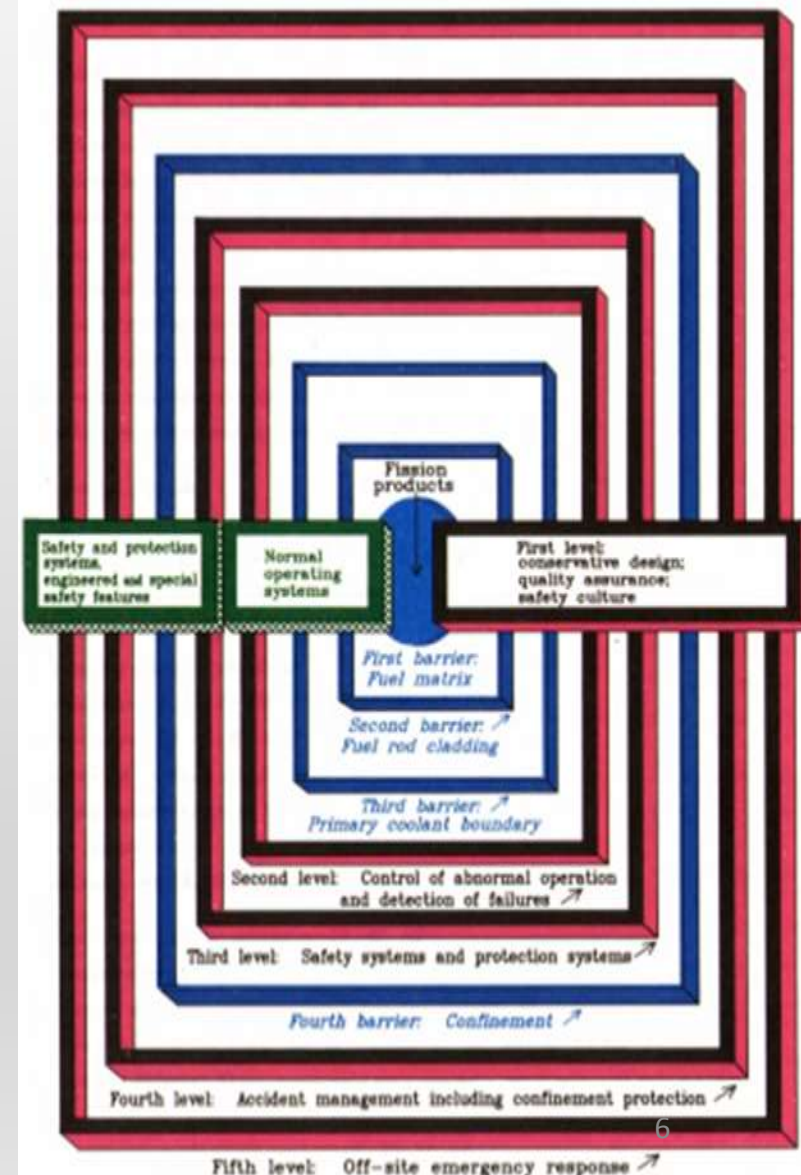
- *Confinement of radioactivity (barriers)*
- *Limits on dose (radioprotection)*
- *Control of nuclear reaction (stop proton beam)*
- *Heat removal from beam dump (cooling system)*



# Safety philosophy (2)

## Defence in depth for SPES (beam dump config.):

1. *Primary barrier: Cooling System and Vacuum*
2. *Local shielding around BD*
3. *Concrete wall of A6 bunker*
4. *Ventilation system (dynamic barrier)*



# *Beam dump safety system*

Logical  
scheme

Identify the top event

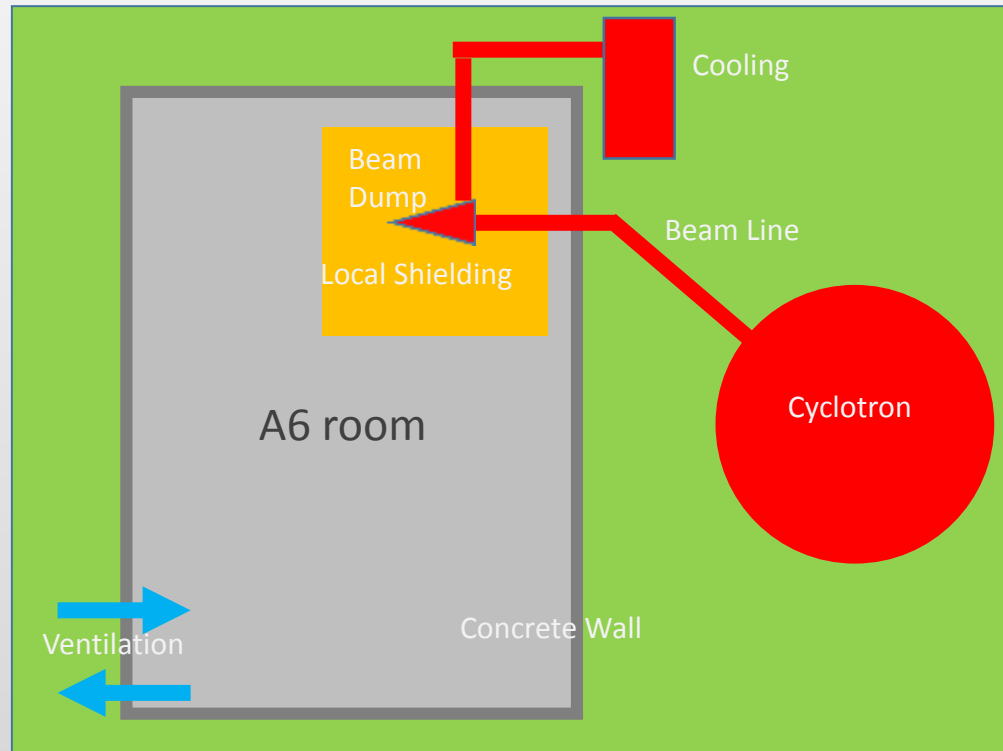


Identify the physical quantities that control the evolution of accident



FEM simulation and theoretical model to evaluate the interlock values

# Beam dump safety system



## Goal of the Beam Dump Safety System

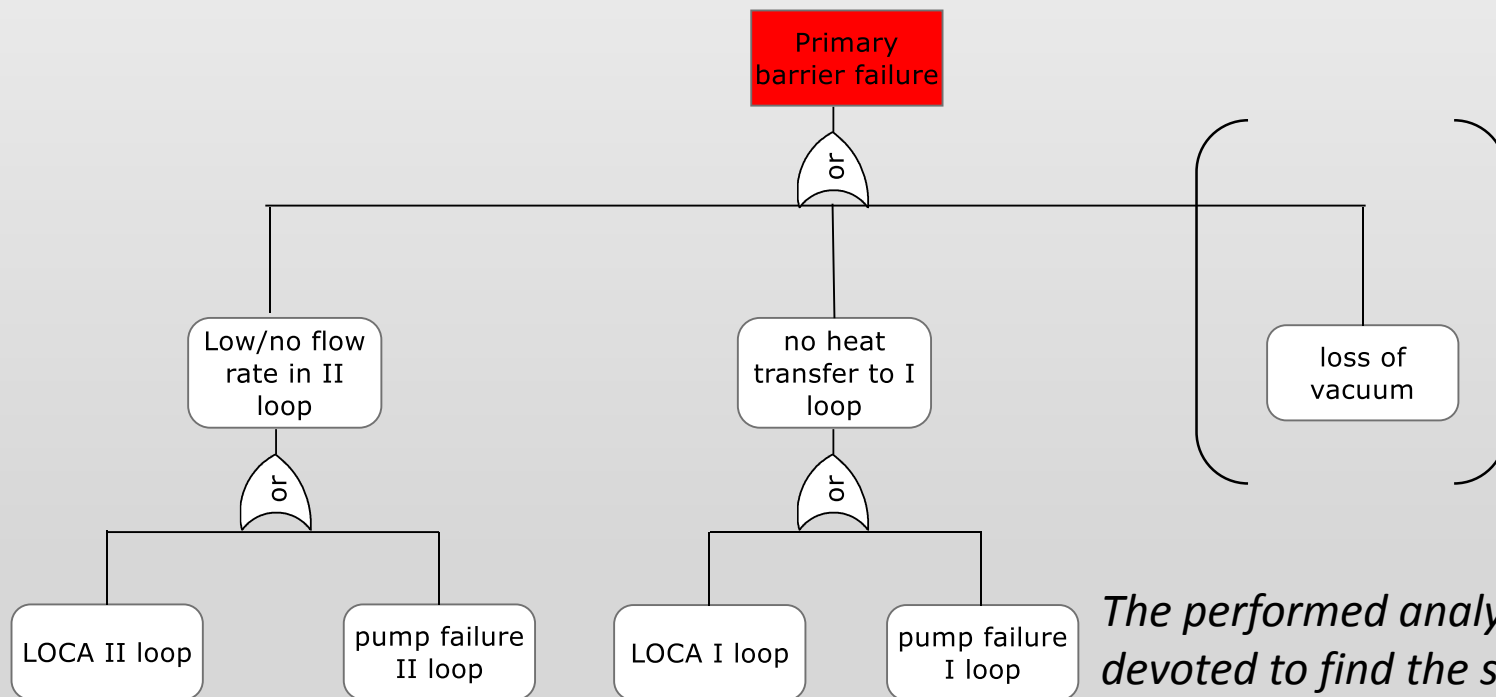
To confine:

1. the interaction of protons with matter
2. the activated products coming from this interaction inside the *primary boundary system*.



# Beam dump safety system

The right question: *How can the primary barrier fail?*



*The performed analysis is devoted to find the shutdown signals coming from cooling system*

# Beam dump safety system: Temperature

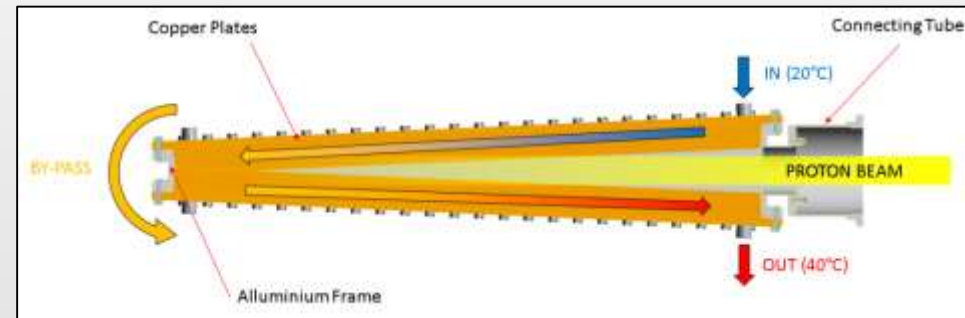
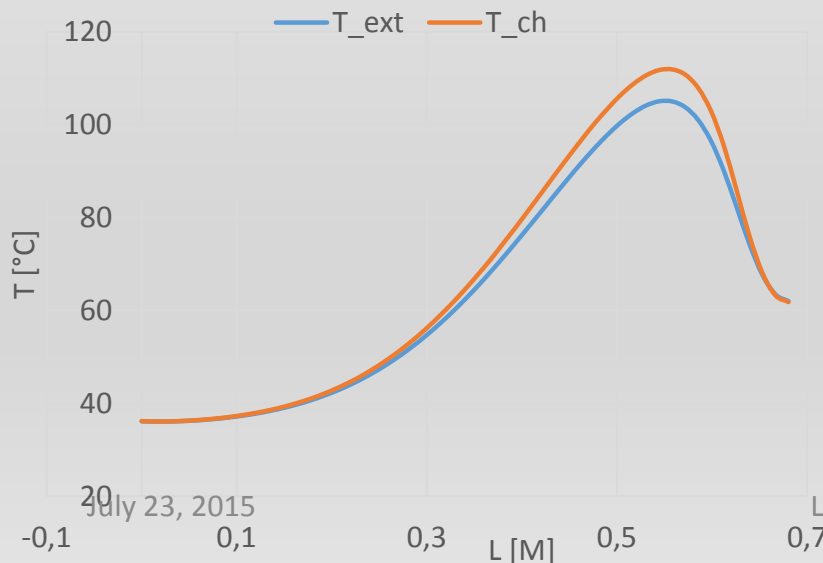
## Thermal analysis: FEM results

Goal: define the hot spot during the operating condition

Steady state analysis

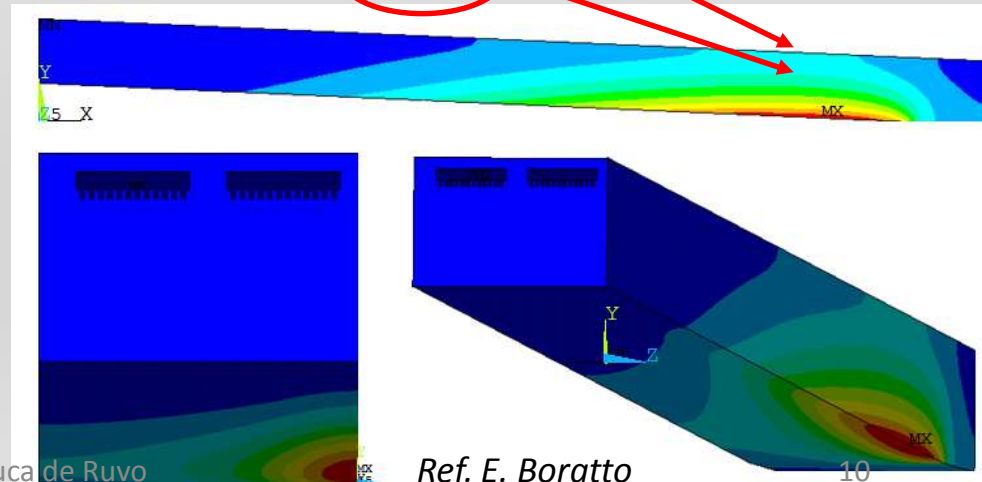
HP:

- Water HTC: 7000 W/°C m<sup>2</sup>
- Fully developed turbulent flow
- Thermal power: 52.5 kW



Hot spot:

- $T_{ext}^{max} = 105\text{ °C}$
- $T_{ch}^{max} = 112\text{ °C}$



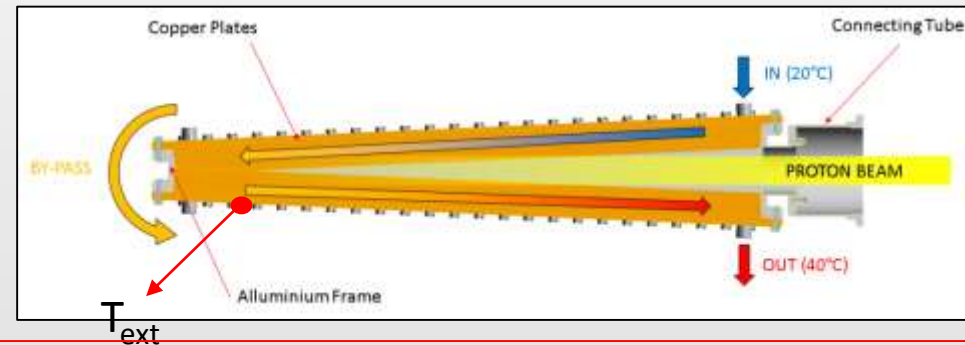
Ref. E. Boratto

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# Beam dump safety system: Temperature

H2O sat

T [°C]	P [MPa]
100	0,101
105	0,120
110	0,143
115	0,169
120	0,199
125	0,232
130	0,270
135	0,313
140	0,361
145	0,416
150	0,476
155	0,543
160	0,618



According to FEM:

$$T_{termc} = T_{ext}^{max} = T_{ch}^{max} - \Delta T$$

Measuring T by ext. termocouple it is possible to estimate the temperature inside the channel wall.

Constrains in temperature:

1. T wall in cooling channel in the hot spot < T **saturation of water** (low HTC)
2. T Indium gasket < T **melting In** (156°C)

# Beam dump safety system: Temperature

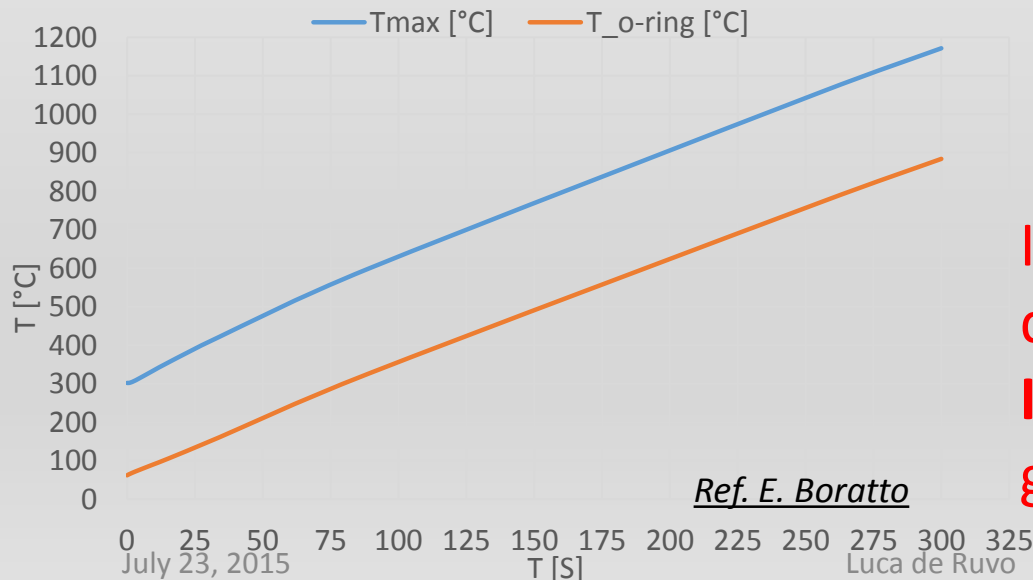
## Thermal analysis: FEM results

Goal: to estimate the time available  
before having a primary barrier failure in  
case of LOCA.

Transient analysis

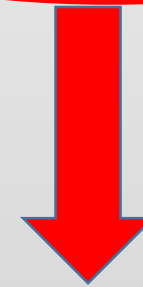
HP:

- No water in channels



Hot spot:

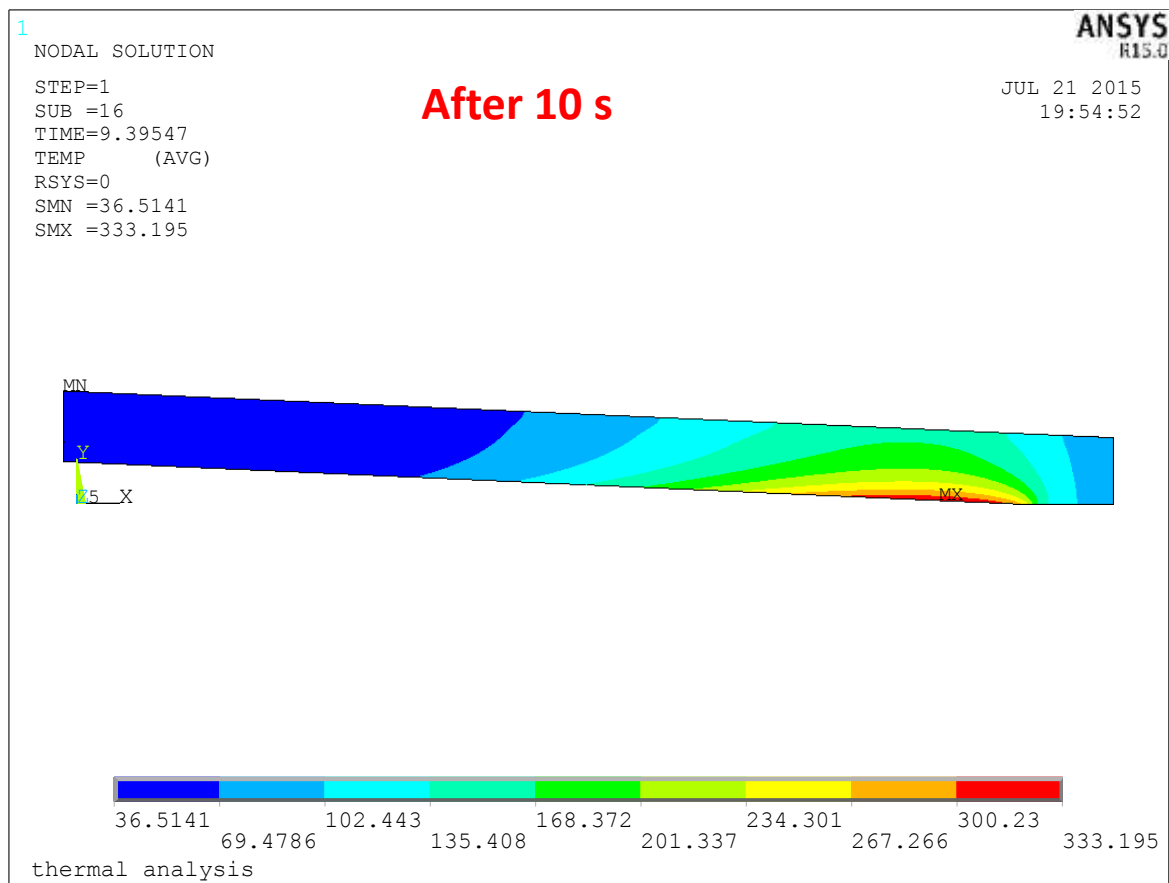
- $T_{Cu}^{melt}$  after 300 s
- $T_{In}^{melt}$  after 10 s



In case of *critical heat flux* the  
driving parameter is the  
**Indium temperature** (vacuum  
gasket)

# Beam dump safety system: Temperature

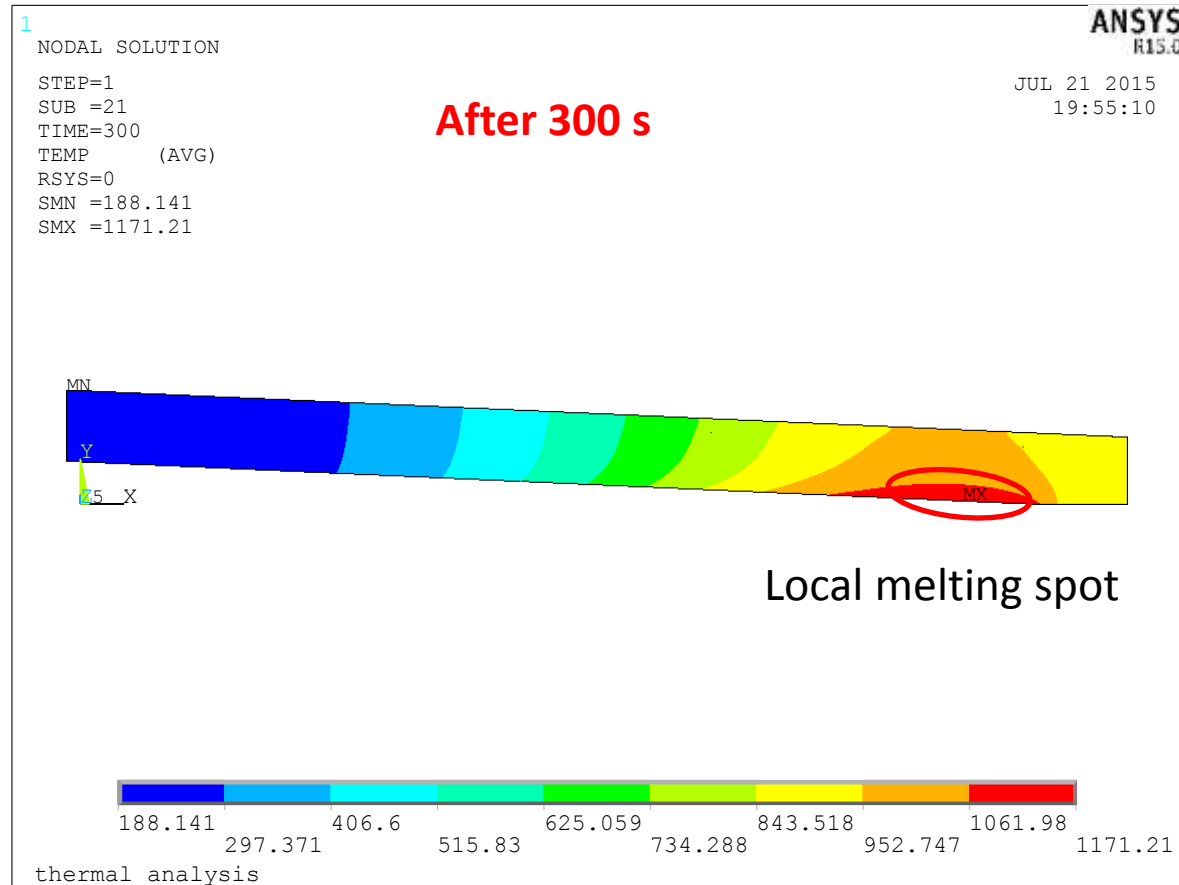
## Thermal analysis: FEM results



Ref. E. Boratto

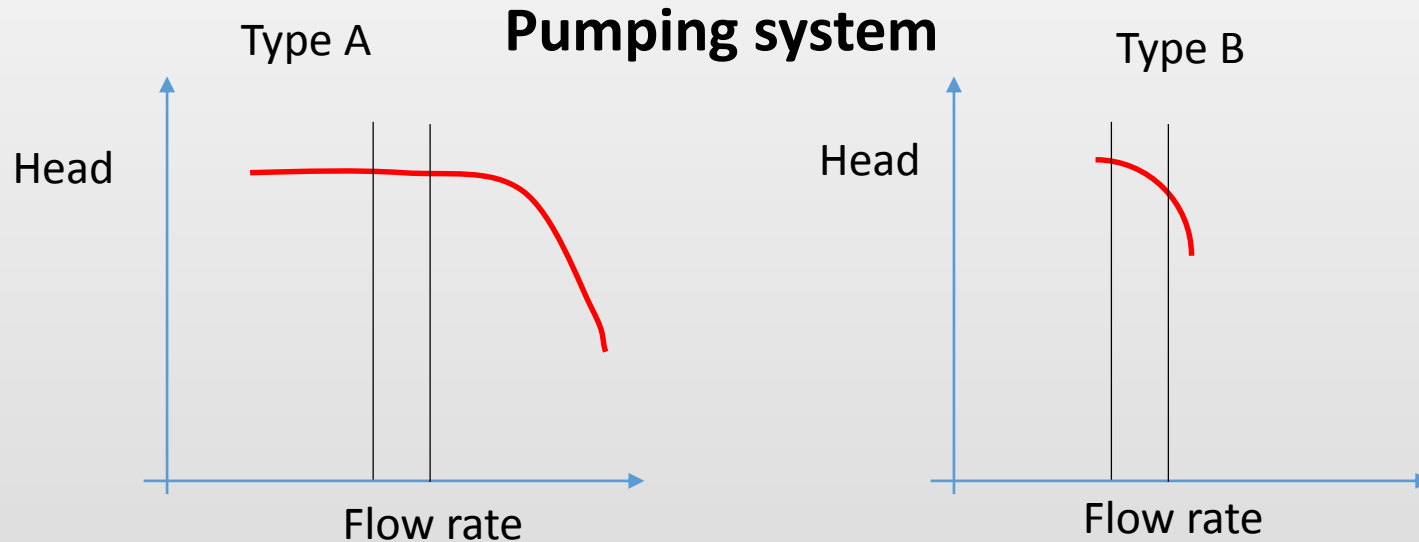
# Beam dump safety system: Temperature

## Thermal analysis: FEM results



Ref. E. Boratto

# Beam dump safety system: Pressure

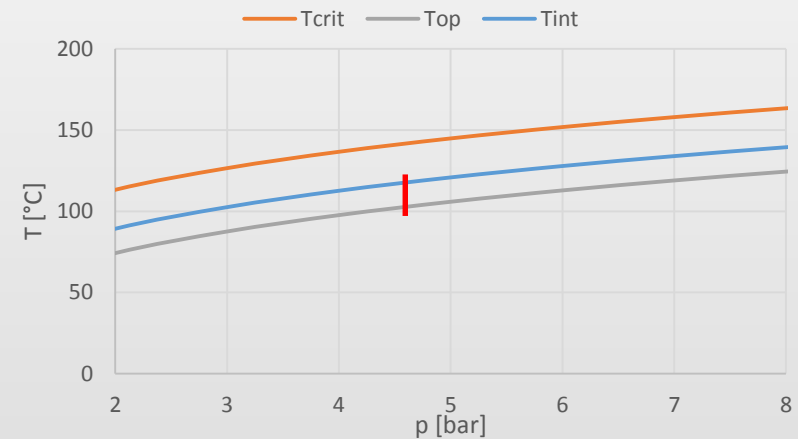
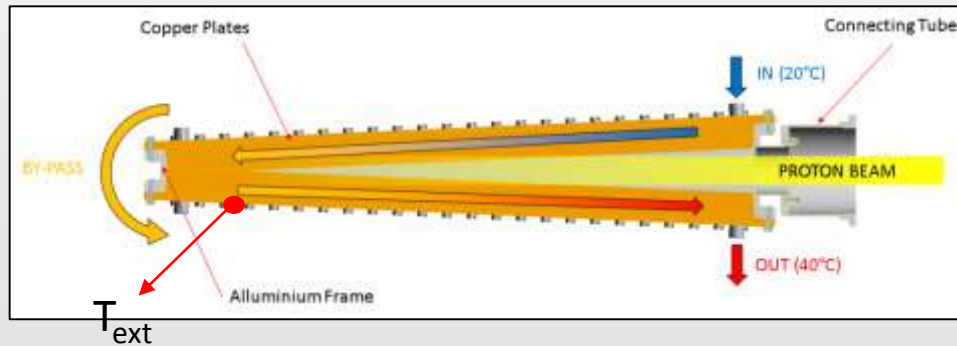


What should drive in the choose of pumping system (safety by design)

Hp: LOCA between pump and beam dump (worst case):

- A. Small variation in  $m$  doesn't produce variation in  $p$ , if type A pump (best stability)
- B. Small variation in  $m$  produces variation in  $p$ , if type B pump (possible instability)

# Beam dump safety system: summary



1.  $T_{ext} < T_{ext \max}$
  2.  $P > P_{\min}$
  3. Cooling Flow rate  $> \dot{m}_{\min}$  ( $P_{th} = c_p \dot{m} (T_{out} - T_{in})$ )
- } redundancy



## Shut down of cyclotron

- High  $T_{ext}$
- Low pressure water channel
- Low cooling flow rate



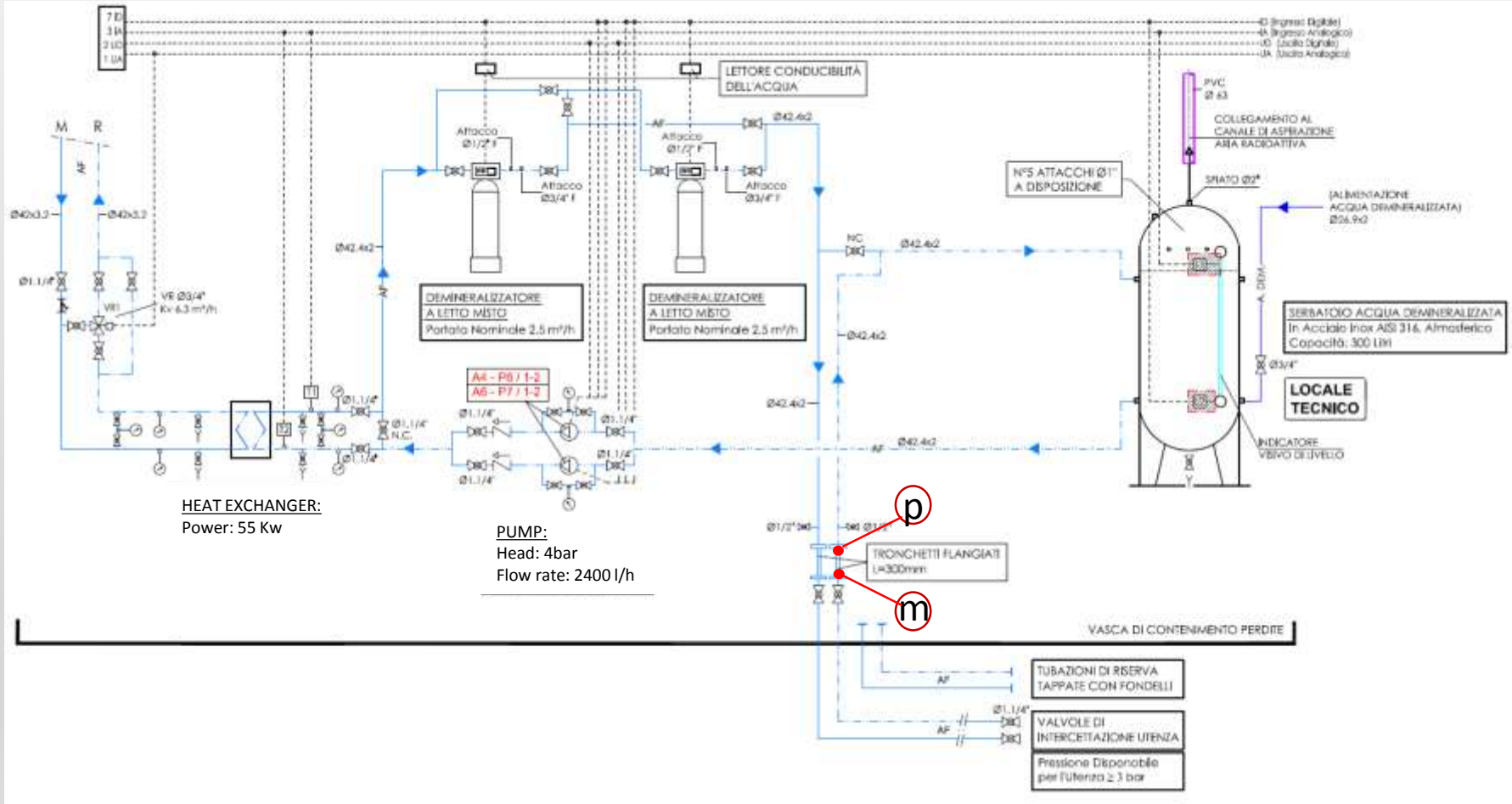
# Beam dump safety system

## Definition of the interlock values for the cooling system

Physical quantity	Measuring device	Location	Operational value	Critical threshold for safety	Interlock set point
Pressure	Barometer	Cooling loop	5 bar	4 bar	4,5 bar
Flow rate	Flowmeter	Cooling loop	2400 l/h	1900 l/h	2200 l/h
Temperature	Termocouple type K	Beam dump	105 °C	144 °C	120 °C

# Beam dump safety system

## Where they are placed?



# *Critical safety aspects: accident scenario*

## Failure of Heat Exchanger

# Critical safety aspects: accident scenario

Plate Heat Exchanger (AISI 316L, stainless steel brazed)

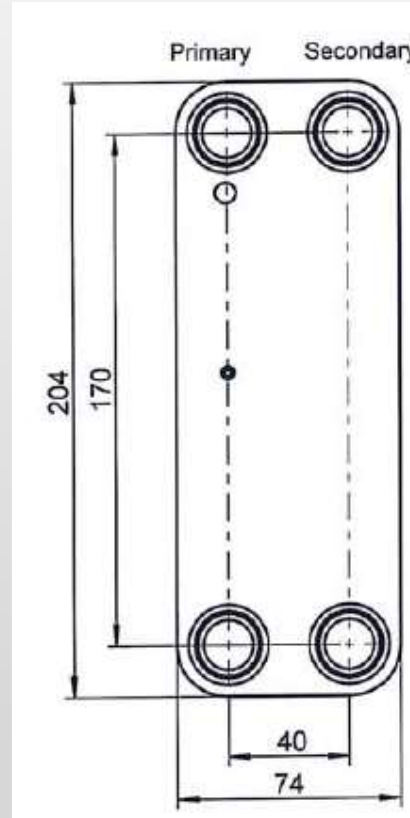
I loop:

- Clean water
- $P_{nom} = 3 \text{ bar}$

II loop:

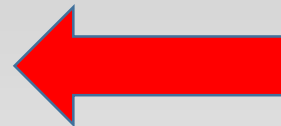
- Radioactive water
- $P_{nom} = 5 \text{ bar}$

Thermal power: 55 kW



At the EoB (some days) water is highly activated (**some kBq/g**)

In case of HEX failure some radioactive water could contaminate the I loop



# Critical safety aspects: accident scenario

How credible this scenario is?

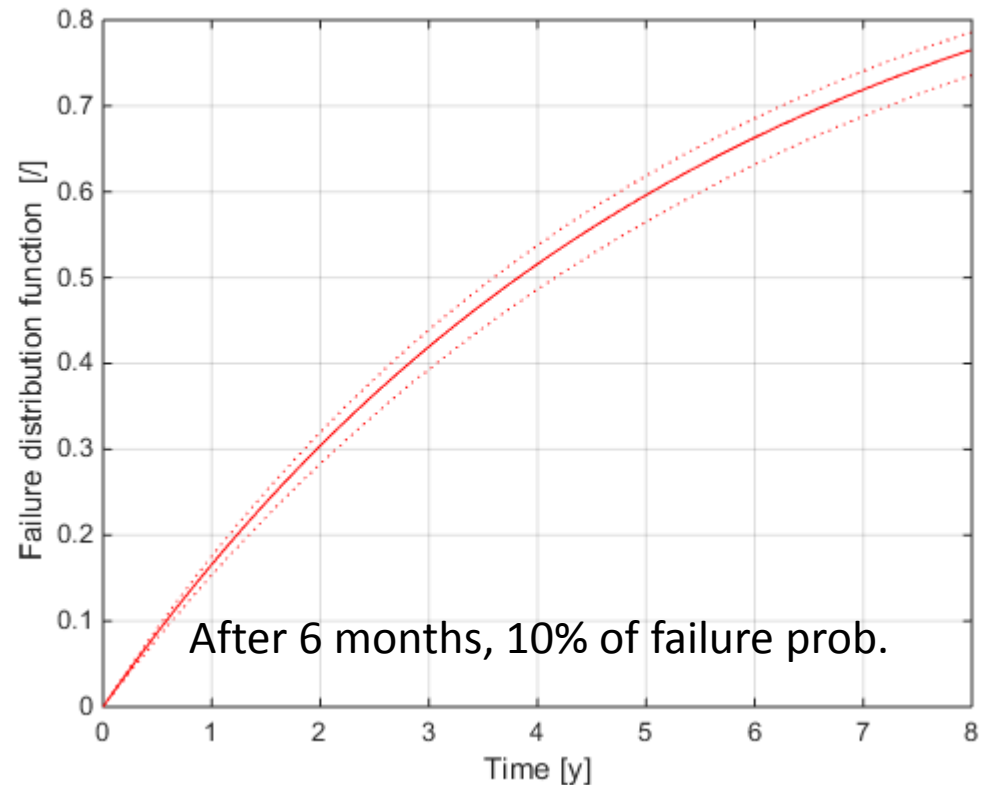
Equipment	Mean failure rate [ $10^{-6}/h$ ]	Range [ $10^{-6}/h$ ]
Plate HEx	20,7	19 - 22

## Note on methodology

The exponential distribution is usually applied to data in the absence of other info and it is the most widely used in reliability work:

$$F(t) = 1 - e^{-\theta t}$$

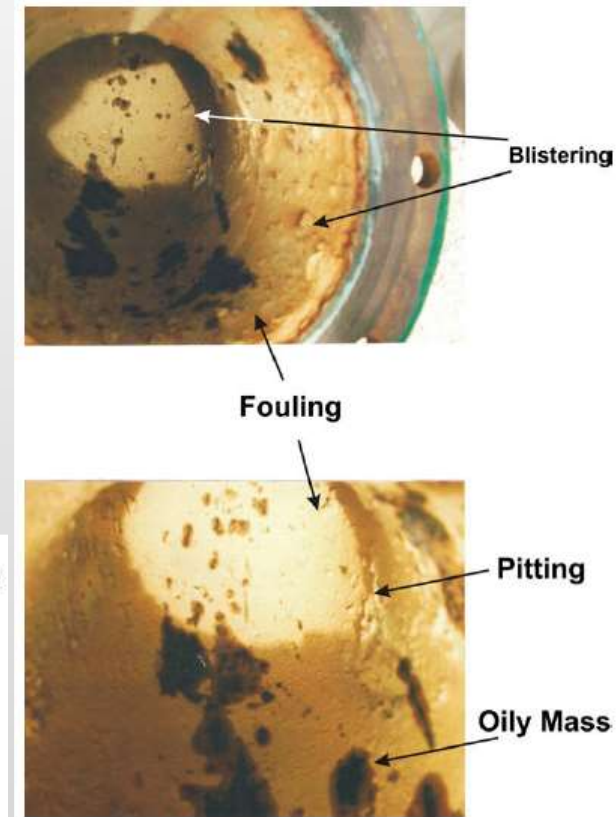
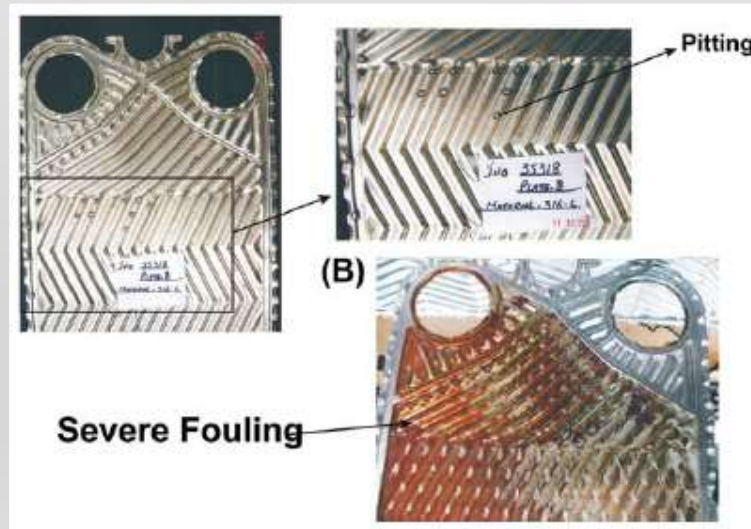
Data and theory from **Loss Prevention in the Process Industries: Hazard Identification - Lees**



# Critical safety aspects: accident scenario

## What causes heat exchanger failure?

- Fouling
- Corrosion (pitting, stress corrosion,...)
- Metal erosion
- Water hammer
- Vibration fatigue
- Thermal fatigue



Pictures from *Engineering Failure Analysis*  
17 (2010) 886–893

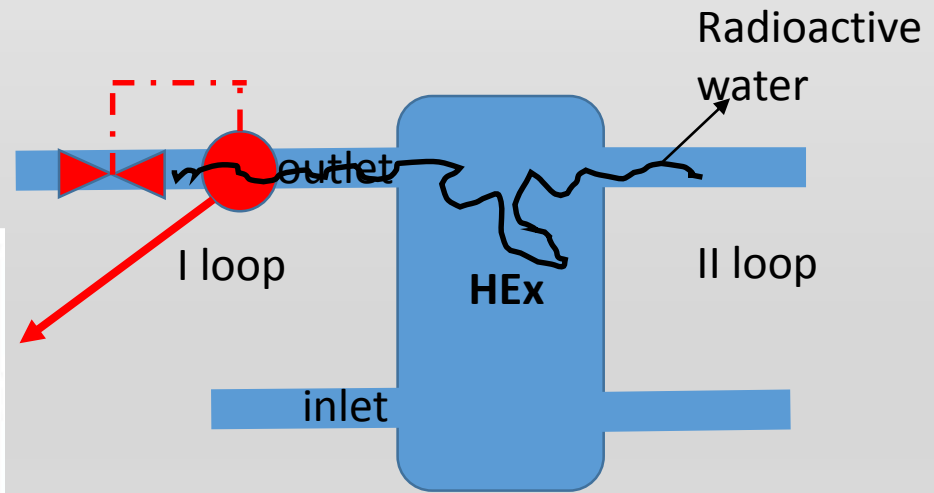
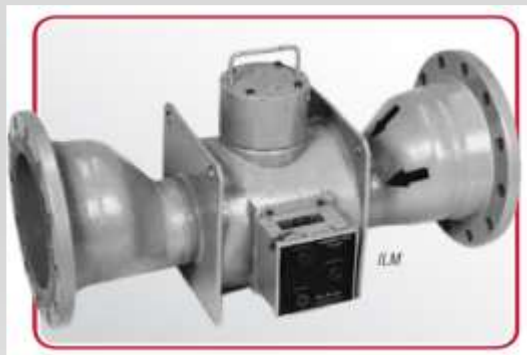
# Critical safety aspects: accident scenario

## Actions to implement for improving HEx life ?

- Water ph: 7 – 8,5
- Chloride < 5 ppm
- Filter to prevent sediment build-up
- Monitoring the the cooling water flow rate to prevent fouling
- Visual inspection (if possible)
- Chemical and/or mechanical cleaning (if possible)

## .... and if everything goes wrong?

### In-line gamma monitoring of I loop



# Safety analysis on beam dump cooling

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**Thanks for attention**